

## Reasoning Barley Grain Drying Modes for Vacuum-Infrared Drying Machines

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**Abstract:** The study describes a construction of a new batch cereal grain drying machine. The machine operation is based on combined drying consisting in infrared heating at the ambient pressure in vacuum. Then grain is dried by the convective method and cooled by the ambient air flow when grain is discharged from the drying chamber. Experimental studies proved that the highest possible temperature of barley grain heating that doesn't result in protein denaturation is 70°C. There is a regression dependence of moisture removal on preheating and vacuum heating time, vacuum volume and the initial moisture content of barley grain resulted from the Box-Behnken second-order design for four factors. Mathematical models of drying mode optimization are developed. Parameters of a barley seed drying mode are found when solving the problem of energy cost optimization and average drying rate. Barley grain drying enhancement is found to be achieved by cutting operating costs and increasing vacuum volume.

**Key words:** Grain drying, barley grain, grain moisture, dryer, infrared heating, vacuum

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### INTRODUCTION

Climatic conditions of many European countries including Belarus, Kazakhstan, Baltic States and most territory of the Russian Federation aren't favorable to harvest grain crops at normal amount of moisture (Semenov, 2012). In some years the share of grain to be dried is 80% (Ginzburg, 1960; Moreno *et al.*, 2017). Drying machines of different types and operation modes are used for these purposes.

Most of the drying methods are based on thermal action that can devitalize barley grain and its food qualities.

Designs of different drying machines for barley grain are reasonable to consider in terms of reduced temperature and mechanical effect, higher drying rate, lower energy and capital costs, less impact on the environment.

The most widespread drying systems used in agriculture are convective grain dryers as the most effective and simple. But they are of high cost, steel intensity and energy consumption (Ginzburg, 1960;

Lykov, 1968; Sutyagin *et al.*, 2017). Specific energy consumption of tower dryers operating on liquid and gas fuel mustn't be over 4.56 MJ/kg of evaporated moisture when drying food and industrial grain crops and 5.74 MJ/kg when drying seed grain (Anonymous, 2008). In fact, convective dryers, operating without heat recovery, expend up to 6 MJ/kg of evaporated moisture due to the fact that most of the heat is carried away irretrievably by the drying agent. When heat is recovered, the specific energy consumption of convective dryers can be reduced to 3.24 MJ/kg (Sorochinsky, 2011) that corresponds to 77.5% of the thermal efficiency.

In the Russian Federation tower and convective drum dryers have a significant disadvantage. There is grain damage in seed material drying. Moreover, grain in tower dryers is overheated that results in protein denaturation in the seed embryo (Li *et al.*, 2017).

Convective grain dryers, regardless of their design, consume energy inefficiently and have low drying rate for the dryable material has a temperature gradient (Jokiniemi *et al.*, 2015). This disadvantage is partly eliminated by alternating heating of the wet material with its cooling (Jokiniemi *et al.*, 2015).

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Microwave and thermal radiation drying methods are characterized by penetration of electromagnetic waves inside of the dryable material that provides its internal heating (Rogov, 1988). Heating from the inside of the material is a distinct feature of microwave drying (Zhao *et al.*, 2017). Therefore, the thermal diffusion of moisture from the center to the surface of the body increases the speed of microwave drying. However, during the microwave drying process when there is no control on temperature and moisture content inside the grain there is a high probability of the embryo death due to possible local overheating.

In thermal radiation drying Infrared (IR) Rays are directly absorbed by the product, thereby providing a more uniform heating of the material in depth in comparison with convective drying (Ginzburg, 1960; Lykov, 1968; Rogov, 1988). It results in a decrease in the temperature gradient and the transfer of steam from the inside to the outside under the action of the total pressure gradient (Darvishi, *et al.*, 2013; Bettega *et al.*, 2014; Zhao *et al.*, 2017). Compared with microwave radiation, IR radiation has a more gentle temperature effect on grain, since, it is less able to warm the inner part of the grain and thus is more acceptable to dry barley grain for seed and brewing purposes. It should be taken into account that higher temperature of infrared heating can lead to damage of the grain embryo. In turn, forced decrease in the heating temperature leads to a decrease in the drying rate and, as a result to the longer drying process, lowers performance of the dryer and higher energy consumption (Rogov, 1988; Li *et al.*, 2014).

After many years of improvement of all the above mentioned traditional methods of grain drying and upgrade of drying systems it is possible to state that there are practically no more ways for their further development. Therefore, the most promising is development of combined methods of drying. They have more reserves to increase efficiency of the grain crop drying process. The idea of combined drying of wet materials is not new. Using several methods of drying in different combinations is proved to be efficient by numerous studies (Ginzburg, 1960; Lykov, 1968; Anonymous, 2008). There are methods when different types of drying take place in the drying machine at once or one after another (Ginzburg, 1960; Lykov, 1968; Zhidko *et al.*, 1982).

Combined contact and convective drying is being studied under the supervision of Professor Kurdjumov V.I. at Ulianovsk State Agrarian University (Ivanovich *et al.*, 2013). The main disadvantage of contact drying is direct contact with the hot heat exchange surface that results in overheating of the material.

At Bashkir State Agrarian University Ganeev (2011) and Fayzrakhmanov (2015) study microwave radiation in combination with convective drying.

Scientists of the Federal University of San Carlos Bettega *et al.* (2014) Freire combine microwave and vacuum drying.

As it was said before, a common disadvantage of microwave drying is uncontrolled heating of the grain embryo.

At Ryazan State Agrotechnical University named after P.A. Kostychev they conduct scientific researches on drying bee pollen in a vacuum-infrared drying machine that minimizes the duration and energy consumption of the drying process (Byshov *et al.*, 2016).

Evaluating the existing works showed that combined use of infrared radiation and vacuum provides the drying process at low temperatures, removes up to 8% moisture for one operation, reduces the duration of the drying process and its cost (Masalimov and Karimov, 2014).

Taking into account the above mentioned ideas, we decided to use the combined effect of vacuum and infrared radiation with further convective drying of barley grain (Karimov *et al.*, 2016). The noted advantages allow us to consider this direction of development of the technology of post-harvest processing of grain crops to be quite promising (Soares *et al.*, 2016; Manikantan *et al.*, 2014; Maier, 2017).

The aim of the study is to reduce the specific energy costs, increase the barley grain drying speed and quality by developing a vacuum-infrared drying machine and determining the optimal parameters of the drying mode.

## **MATERIALS AND METHODS**

Infrared heating in a vacuum environment is implemented in a vacuum drying unit developed at the Bashkir State Agrarian University. It is of a batch type where air-conditioned grain moisture is achieved at one time of processing (Anonymous, 2011). The drying process is carried out as follows.

The feeder delivers wet bulk material through the hatch 1 to the hopper 2 which is a drying chamber of 0.25 m<sup>3</sup> volume, divided into 3 sections by film-type IR transmitters 3 with a wavelength of 7.4 μm (Fig. 1). The programmable controller of the control unit 4 processes the signal received from the temperature and moisture sensors installed in the drying chamber, activates the IR transmitters and maintains the set temperature of the grain heating. Then the value VE260N vacuum pump 5 is switched on which creates vacuum in the drying chamber 2. After the preset heating time, the material when the screen 6 is open, passes to the air chamber 7 where it is subjected to convective drying by the active air blowing fan 8. As a result, dust and light weed seeds are blown out through the discharge opening 9 and the dried material moves along the slanting pan of the chamber 7 for discharge.

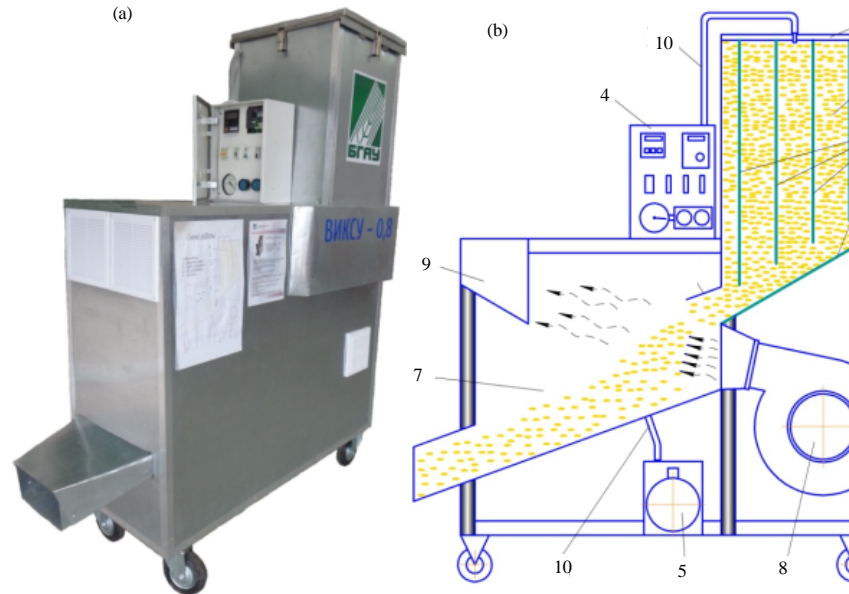


Fig. 1: Vacuum-infrared drying unit: a) General view and b) Schematic diagram; 1) Hatch; 2) Bulk material hopper; 3) IR transmitter; 4) Control unit; 5) Vacuum pump; 6) Screen; 7) Air chamber; 8) Fan; 9) Bulk material discharge and 10) Vacuum pipe

In the drying chamber the moist material is heated to a preset temperature and IR radiation heats the grain inner part intensively enough for temperature gradient not to hinder diffusion of moisture from the centre to the surface of the material in contrast to convective drying. The vacuum created in the drying chamber, firstly, increases the pressure gradient and secondly, reduces the temperature required to evaporate moisture in the material. Thus, infrared radiation in vacuum environment accelerates the grain moisture removal process at a gentle temperature. The final drying of the material is carried out in the air chamber by blowing with a drying agent which is atmospheric air at 20-25°C. The moisture that has passed from the material is forced out through the discharge opening 13.

The previous experiment found the material layer per each IR transmitter to be 25 mm thick provided the grain is equally heated. Thus, the distance between adjacent IR transmitters is 50 mm.

At a constant vacuum pump capacity of 170 dm<sup>3</sup>/min the vacuum value was changed with the help of an adjustment mechanism by changing the atmospheric air intake channel throat. The vacuum gauge incorporated in the control unit monitored the vacuum value.

A screw type feeder T-403/2 with up to 15 t/h capacity and 2.2 kW power is used to deliver the grain to the hopper.

The barley seeds of the “Mikhailovsky” cultivar with the initial germination of 97.8 % were used. Samples of the grain dried in a vacuum infrared dryer were taken at the

beginning in the middle and at the end of the discharge in each experiment which corresponded to the different arrangement of the grain in the drying chamber. Electrical moisture meter “Fauna M” was used to determine the moisture value of the grain in each sample by the express method. The values were then averaged. Grain was wetted and subjected to convective drying at the drying agent temperature of no more than 25°C to obtain the initial grain moisture.

Samples to determine seed germination capacity were taken in line with different location of the grain in the drying chamber. Germination capacity of barley seeds was determined based on standard procedures (Anonymous, 2011; Friesen *et al.*, 2014).

Three or four factor experiments used Pesochinsky (Martynov, 2018; Pinchuk, 2008) and Box-Behnken (Martynov, 2018; Adler *et al.*, 1976) second-order non-compositional designs with three factor variation levels (-1; 0; +1) as the basis for mathematical modeling. The experiments provided three-and fourfold replication, the order of the experiments was randomized.

Student’s test was used to determine regression ratios and Fisher’s ratio test at 0.05 significance level was used to identify the adequacy of mathematical models in the statistical experimental data processing.

## RESULTS AND DISCUSSION

Efficiency of the described vacuum infrared drying machine depends on the regular drying modes, namely the

Table 1: Parameters of the experiment design of the study on grain germination

Design parameters	Coded value	Factor values at the design points		
		T <sub>max</sub> (°C)	t (min)	W <sub>i</sub> (%)
Zero level	0	80	17.5	19
Variation range	1	15	12.5	3
Upper level	+1	95	30.0	22
Lower level	-1	65	5.0	16

maximum temperature of grain heating, the vacuum value, the heating time in and without vacuum. The effect of these parameters on the barley drying process is still to be considered. Therefore, experimental studies were aimed at providing the base for operation modes of drying barley grain for seed production and brewing purposes.

The zero degree limit of protein denaturation can be used as a basis for selecting drying modes (Zhidko *et al.*, 1982). The factors T<sub>max</sub>-maximum temperature of heating the IR transmitter surface, t-heating time, W<sub>i</sub>-the initial grain moisture content were taken as the three main ones affecting the viability of the grain after drying. A dependence of an increase in thermal stability of the grain upon a decrease in the grain moisture content and the time of high temperatures was used as an initial fact (Zhidko *et al.*, 1982).

Factor variation ranges were taken based on the study of the relevant literature on infrared radiation and vacuum type drying (Byshov *et al.*, 2016) as well as drying technological requirements and drying machine design features. Table 1 demonstrates the range limits of factor variation.

A three factor experiment was performed with threefold replication to investigate the effect of the factors on the germination capacity of barley seeds G in accordance with (Anonymous, 2011; Friesen *et al.*, 2014) (Table 2).

After heating the grain was dried under atmospheric conditions to moisture content of 14% and then barley seed germination capacity was tested.

Statistical experimental data processing showed that neither the heating time from 5-30 min, nor the initial moisture content of the seeds in the 16-22 % range has a significant effect on the thermal stability of barley seeds. After excluding insignificant regression ratios, the following relationship of the barley seed germination capacity and the decoded T<sub>max</sub> value was obtained:

$$G = -294.15 + 11.7565T_{max} - 0.0887T_{max}^2 \quad (1)$$

The regression dependence provides an adequate description of the test data at 0.05 significance level it has a multiple correlation ratio R = 0.917 and is represented graphically in Fig. 2.

Table 2: The matrix of the Pesochinsky three-factor design

Experiment number	Factors			Germination capacity G (%)		
	T <sub>max</sub>	t	W <sub>i</sub>	G <sub>1</sub>	G <sub>2</sub>	G <sub>3</sub>
1	+1	+1	0	23	4	15
2	+1	-1	0	30	9	16
3	-1	+1	0	93	98	95
4	-1	-1	0	95	99	92
5	+1	0	+1	45	9	15
6	+1	0	-1	68	15	17
7	-1	0	+1	94	96	91
8	-1	0	-1	98	95	97
9	0	+1	+1	85	58	72
10	0	+1	-1	93	75	84
11	0	-1	+1	90	91	69
12	0	-1	-1	89	93	51
13	0	0	0	91	52	87

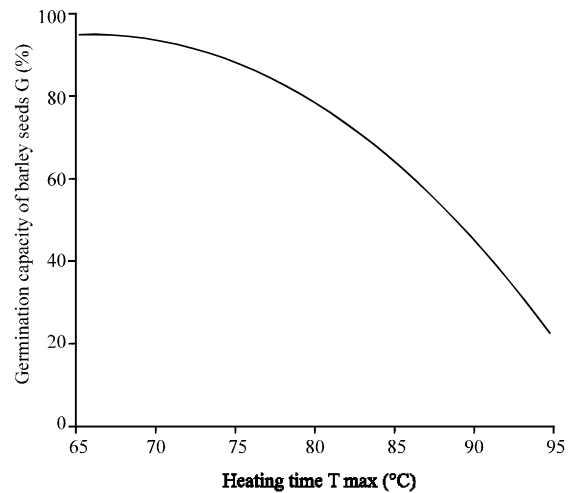


Fig. 2: Dependence of barley seed germination on the IR transmitter surface temperature

It can be seen from Fig. 2 that heating at a temperature higher than 70°C causes a significant decrease in the barley seed germination capacity. Therefore, this value is accepted as the maximum grain heating temperature which ensures maximum drying intensity that does not result in protein denaturation.

The following input parameters were taken in the experiment on establishing the optimal mode of barley grain drying: the vacuum value H; heating time without vacuum (preheating time) t<sub>1</sub>; heating time in vacuum t<sub>2</sub>; initial moisture content of grain W<sub>i</sub>. The output parameter was the value of the moisture removal DW. The following factor variation ranges were taken: H (20, 80 kPa), t<sub>1</sub> (0; 60 min), t<sub>2</sub> (6, 60 min), W<sub>i</sub> (16, 22%). The experiment was performed under the Box-Behnken design for four factors with a four fold replication (Table 3).

During the experiments, the grain was heated not higher than 70°C. A thermostat was used to maintain the required temperature of grain heating. Figure 3 shows one

Table 3: Matrix of the experiment design on establishing the mode of barley grain drying in a vacuum infrared dryer

Experiment number	Factors				Moisture removal DW (%)			
	H	t <sub>1</sub>	t <sub>2</sub>	W <sub>1</sub>	DW <sub>1</sub>	DW <sub>2</sub>	DW <sub>3</sub>	DW <sub>4</sub>
1	+1	+1	0	0	5.00	4.13	4.00	4.50
2	+1	-1	0	0	2.04	2.50	2.47	2.40
3	-1	+1	0	0	2.20	2.50	1.74	2.10
4	-1	-1	0	0	1.65	1.05	1.40	1.30
5	0	0	+1	+1	5.04	5.90	5.60	5.23
6	0	0	+1	-1	1.30	1.70	2.05	1.80
7	0	0	-1	+1	2.30	2.70	1.80	2.33
8	0	0	-1	-1	0.05	0.40	0.05	0.10
9	0	0	0	0	2.70	2.21	2.00	2.43
10	+1	0	0	+1	5.10	5.60	5.90	5.63
11	+1	0	0	-1	1.85	1.50	1.15	1.53
12	-1	0	0	+1	3.58	3.10	3.80	3.43
13	-1	0	0	-1	0.75	1.00	0.35	0.60
14	0	+1	+1	0	4.35	3.60	3.97	4.10
15	0	+1	-1	0	1.44	1.20	0.80	1.03
16	0	-1	+1	0	2.20	2.84	2.31	2.53
17	0	-1	-1	0	0.20	0.05	0.09	0.07
18	0	0	0	0	2.10	2.74	2.20	2.43
19	+1	0	+1	0	5.40	4.90	4.50	5.03
20	+1	0	-1	0	0.64	1.25	0.90	0.70
21	-1	0	+1	0	2.50	2.00	2.80	2.40
22	-1	0	-1	0	0.61	0.90	0.30	0.50
23	0	+1	0	+1	5.80	5.10	4.70	5.20
24	0	+1	0	-1	1.40	1.67	1.00	1.30
25	0	-1	0	+1	2.60	3.10	3.50	3.07
26	0	-1	0	-1	0.75	0.45	0.90	0.63
27	0	0	0	0	2.71	2.20	2.00	2.43

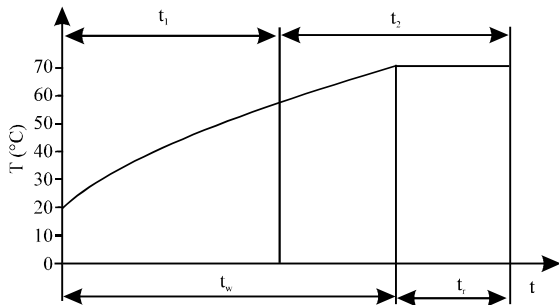


Fig. 3: Graph of the barley grain heating process in a drying machine

of the possible options for heating the grain. The period of grain heating, characterized by a temperature rise to a  $T_{max}$  value is  $t_w$ . During this period, the IR transmitters operate at full power. Then, during the period  $t_r$  the IR transmitters go into a periodic operational mode and maintain a constant grain heating temperature  $T_{max}$  with the help of the heat regulator. Depending on  $t_1$  and  $t_2$  values grain may and may not reach the maximum temperature  $T_{max}$  both during the time period  $t_1$  and  $t_2$  this case is shown in Fig. 3.

Statistical processing of the experimental data Table 3 resulted in the following regression equation in the decoded form:

$$DW/W_1 = b_1 + b_2 H + b_3 t_1 + b_4 t_2 + b_5 W_1 + b_6 H t_1 + b_7 H t_2 + b_8 t_1 W_1 + b_9 t_2 W_1 + b_{10} H W_1 + b_{11} H^2 + b_{12} t_2^2 + b_{13} W_1^2 \quad (2)$$

where,  $b_1, b_2, \dots, b_{13}$  are regression ratios: 0.1985; -0.003944; -0.0026953; -0.0005455; -0.02336; 0.00001857; 0.00003635; 0.00015467; 0.00014191; 0.0001181; 0.0000124; -0.0000213; 0.0007684.

The multiple correlation ratio was  $R = 0.979$ . This mathematical model provides adequate description of the entire experiment area and allows examining the effect of drying mode on a number of optimization parameters. Figure 4 and 5 demonstrate graphical dependences of the average drying speed on the studied factors:

$$DW/t = f(W_1, H, t_1, t_2); t = t_1 + t_2 + t_r + t_b \quad (3)$$

Where:

$t_r$  = Time of grain charge into the drying chamber is taken for 1 min

$t_b$  = Time of grain discharge or time of air blowing of grain by the fan is taken for 7 min

An analysis of these relationships showed that the higher the initial moisture content of the grain, the higher is the average barley grain drying speed in a vacuum infrared dryer. Shortening of the grain heating time without vacuum  $t_1$  and a certain time value of grain heating in vacuum  $t_2$  produces more intensive drying.

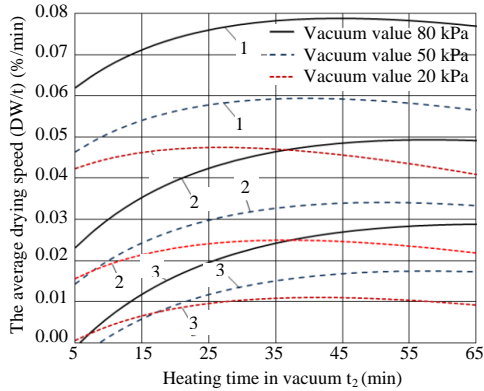


Fig. 4: The dependence of the average drying speed on the heating time in vacuum  $t_2$  the vacuum values at  $t_1 = 30$  min and the initial moisture content of the grain at: 1- 22%; 1-2-19%; 3-16%

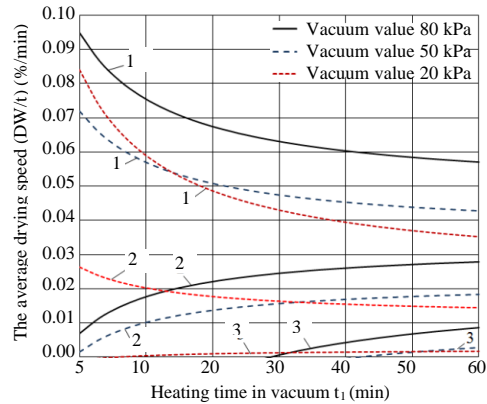


Fig. 6: Dependence of the average drying speed on the heating time without vacuum  $t_2$  vacuum values  $H$  at  $t_1 = 0$  and the initial moisture content of the grain at: 1-022%; 2-19%; 3-16%

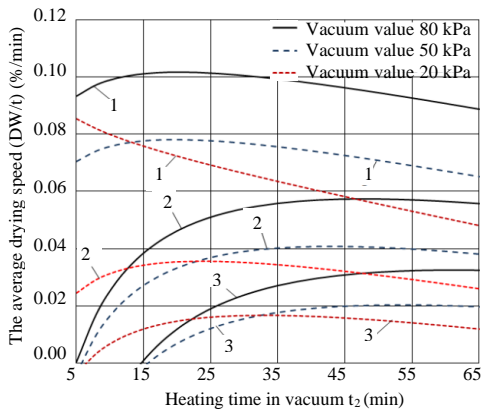


Fig. 5: Dependence of the average drying speed on the heating time in vacuum  $t_2$  vacuum values  $H$  at  $t_1 = 0$  and the initial moisture content of the grain at: 1-22%; 2-19%; 3-16%

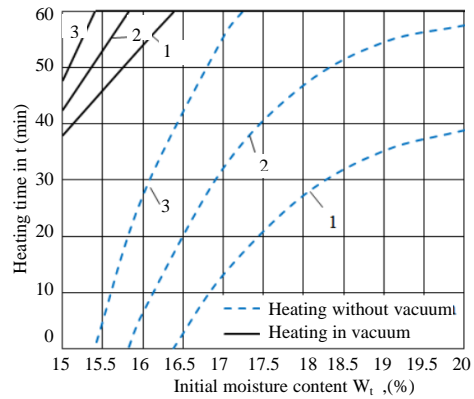


Fig. 7: Optimum grain heating time without vacuum  $t_1$  and in vacuum  $t_1$  depending on the initial moisture content of the grain  $W_1$  at vacuum values, kPa: 1-80; 2-70; 3-60

Further extending of time  $t_2$  leads to a decrease in the average drying speed due to a reduction in the moisture content of the grain. Increasing the vacuum  $H$  causes an increase in the average drying speed.

It should be pointed out that the final moisture content of the grain does not correspond to the specified moisture  $W_f$  at the accepted values  $W_i, H, t_1, t_2$  the same is true for the function extreme values presented in Fig. 4-6. It would be therefore useful to achieve the required final moisture value  $W_f = 14\%$  in the drying process in order to solve the task of optimizing the parameters  $H, t_1, t_2$  which ensure the maximum average drying speed of grain of different moisture  $W_i$ . This will shorten the total drying time of the grain and increase performance of the drying machine.

“Search solution” add-in in MS Excel helped to solve the task of optimizing the grain drying time at  $W_f = 14\%$ . Figure 7 provides graphical representation of the calculation results.

For example, drying the grain with the initial moisture content  $W_i = 20\%$  requires  $t_1 = 39$  min and  $t_2 = 60$  min at a vacuum value of 80 kPa and  $t_1 = 58$  min at a vacuum value of 70 kPa. Drying the grain with the initial moisture content  $W_i = 16\%$  requires  $t_1 = 0$  to achieve  $W_f = 14\%$  and  $t_2 = 54$  min at a vacuum value of 80 kPa.

In terms of energy the optimum drying mode corresponds to the minimum energy consumption of the drying machine (kWh) ensuring the specified final moisture content of the grain  $W_f$

$$E = [N_{tr}t_r + N(t_{w1} + t_{w2} + k_{i1}t_{r2} + k_{i2}t_{r2}) + N_{\eta}t_2 + N_b t_b / 60] \rightarrow \min \quad (4)$$

Where:

- $N_{tr}$  = Power of the feeder, 2.2 kW
- $N$  = total power of infrared transmitters, 6 kW
- $t_{w1}, t_{r1}, t_{w2}, t_{r2}$  = Time of grain heating up to  $T_{max}$  and periodic infrared transmitter operation for drying periods  $t_1$  and  $t_2$  min, respectively
- $k_{t1}, k_{t2}$  = Time periods of infrared transmitter operation in a periodic mode for drying periods  $t_1$  and  $t_2$ , respectively
- $N_{vp}$  = Power to drive the vacuum pump (kW)
- $N_b$  = Fan power, 1.5 kW

If the grain reached the temperature  $T_{max}$  in the first period at a sufficiently high  $t_1$  in time  $t_{w1}$  infrared transmitters operate at full power  $N$  in this time period and they operate in a periodic mode during the time  $(t_1 - t_{w1})$  and in the second period  $t_2$ . If the grain reaches the temperature  $T_{max}$  only in the second period Fig. 3 then the length of the periodic mode will be  $(t_1 - t_{w1})$ . If the grain temperature does not reach  $T_{max}$  in the second period then  $t_{r1} = t_{r2} = 0$ . Note that time  $t_1 = 0$  in some experiments (Table 3).

During the main experiment, grain heating time up to  $T_{max}$  70°C (thermostat actuation time) and grain temperature at the end of the period when it didn't reach 70°C were additionally recorded in each trial. The following regression equation was obtained after statistical data processing:

$$t_w = -10.02 + 0.74T + 0.1925P - 0.0115W_i P - 0.000983P^2; R = 0.952 \quad (5)$$

Where:

- $T$  = The temperature of grain heating during the full power operation of infrared transmitters (°C)
- $P$  = The absolute pressure in the drying chamber (kPa) which is related to the atmospheric pressure and the vacuum value  $P = P_a - H$

To determine the part of infrared transmitter operating time in a periodic mode an additional experiment was performed. It recorded operation and interruption time of the infrared transmitters. Due to statistical experimental data handling we had the regression Eq. 6:

$$k_t = -0.8323 + 0.1177 W_i + 0.00189H - 0.001984 W_i^2; R = 0.990 \quad (6)$$

Optimal modes of barley grain drying were developed using the Eq. 4, taking into account Eq. 5 and 6. Table 4 shows the optimal modes for drying the grain to the final moisture content value of 14%.

Table 4: Optimal modes of drying barley in a vacuum infrared dryer

$W_i$ (%)	$H$ (kPa)	$t_1$ (min)	$t_2$ (min)	$E$ (kW·h)
20	80	38.8	60.0	9.74
19	80	35.2	60.0	9.24
18	80	27.3	60.0	8.42
17	80	13.1	60.0	7.11
16	80	0.0	54.2	5.54
15	80	0.0	38.0	4.26

The drying modes given in Table 4 are identical to the modes found based on the maximum average grain drying speed. The reasons are as follows. Since, infrared radiation is the bulk of the energy consumption shorter heating time leads to a decrease in total energy required.

The optimal mode of drying barley from 20-14% moisture in the vacuum infrared drying machine for seed production and brewing implies specific energy consumption of 3.14 MJ/1 kg of evaporated moisture which is 1.4 times lower than in the contact convective type drying machine and 1.8 times lower than in convective type dryers (Anonymous, 2008; Sorochinsky, 2011). Vacuum value  $H$  has a direct effect on specific heat required for moisture evaporation in the designed vacuum infrared dryer. Lower vacuum values of up to 50 kPa increase specific energy consumption up to 4.5 MJ/1 kg of evaporated moisture. This is accounted for by the fact that vacuum lowers moisture evaporation temperature. Similarly, vacuum increases pressure gradient and drying speed (Ginzburg, 1960; Bettega *et al.*, 2014; Byshov *et al.*, 2016).

The average speed of drying barley seeds from 20-14% moisture content is 0.056%/min. Drying seeds of lower initial moisture implies lower average drying speed and the speed is 0.042%/min at  $W_i = 18\%$  it is 0.022 %/min at  $W_i = 15\%$  (Ginzburg, 1960; Lykov, 1968; Sutyagin *et al.*, 2017). The results are fully in line with the existing studies on drying grain crops (Atanasevich, 1989; Baum and Rezhnikov, 1983; Lebedev, 1962).

### CONCLUSION

The regression dependence of the barley seed germination on the maximum heating temperature of the IR-transmitter surface is established. It is found that the heating time from 5-30 min and the initial grain moisture content in the 16-22% range do not have a significant effect on the thermal stability of barley seeds. It is proved that the highest possible temperature of barley seed heating that doesn't result in protein denaturation is 70°C.

The mode of grain drying in the vacuum infrared drying machine features the following parameters: maximum grain heating temperature, grain heating time in and without vacuum, vacuum value.

The regression dependence of the moisture removal on the mode parameters of drying barley seeds with different moisture content allowed us to study the drying processes in the vacuum infrared drying machine.

The mathematical models designed to optimize the barley drying operation modes made it possible to determine the minimum specific energy consumption and time of barley grain drying.

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